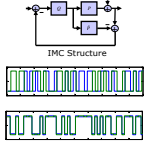


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Summary

- Problem Statement:** Identify model for MIMO controller
 - Satisfy **Integral Controllability**
- Existing Approaches**
 - Well-conditioned systems: Use PRBS inputs
 - Ill-conditioned systems: Use correlated inputs based on uncorrelated **rotated** inputs
- Open Issues**
 - Satisfy input/output **constraints**
 - Assume **well or ill-conditioned** systems?
 - Use **rotated or actual** inputs?
 - How to **distribute energy** to inputs?



- This Work**
 - Systematic approach to MIMO identification experiments subject to integral controllability
 - Main features of proposed approach
 - Satisfies input/output **constraints**
 - Does not require system **characterization as well or ill-conditioned**
 - Recovers existing MIMO input designs as special cases
 - Proposes new MIMO input designs
 - Generalized** rotated inputs
 - Estimates upper bound for experiment duration

Integral Controllability

- MIMO model identified from an identification experiment using a least-squares method
- Model-based control needs integral controllability

Garcia & Morari (1985)
 $\text{Re}[\lambda(GG^{-1})] > 0$ There exists a robustly stabilizing controller with integral action
 G = steady-state gain matrix, true plant
 \hat{G} = steady-state gain matrix, estimate

- A challenge for ill-conditioned systems
- Sub-matrices of MPC model must satisfy

Ill-Conditioned Systems

- Characterized by large condition number and significant gain variation with input directions
- Use of PRBS often leads to models that perform poorly in closed loop

Example: High purity distillation in LV configuration

Uncorrelated inputs
Correlated outputs, strong direction emphasized

$$y = G \begin{bmatrix} u_1 \\ u_2 \end{bmatrix} = U \Sigma V^T m = U \Sigma V^T m + \sigma_1 u_1 v_1^T m + \sigma_2 u_2 v_2^T m \approx \sigma_1 u_1 v_1^T m + \sigma_2 u_2 v_2^T m$$

v_1 strong input direction v_2 weak input direction
 u_1 strong output direction u_2 weak output direction

Koung & MacGregor (1994) Design $\xi = \text{rotated inputs}$ Determine PRBS amplitudes for ξ :
 Based on latest \hat{G} : $y = U \Sigma V^T m$ $\text{var}(\xi) / \text{var}(\xi) = \sigma_i^2 / \sigma_j^2$ $y^T y = u_1^2 \sigma_1^2 + \dots + u_n^2 \sigma_n^2 \leq \gamma$ Implement $m = V \xi$
 $\text{cov}(\xi, \xi) = 0, \tau \neq j$

Highly correlated inputs
Uncorrelated outputs

$$m_1 = v_1 \xi_1 + v_2 \xi_2 \approx v_1 \xi_1$$

$$m_2 = v_1 \xi_1 + v_2 \xi_2 \approx v_2 \xi_2$$

Main Result Integral Controllability Bound

$$\sum_{i=1}^n a_i \sqrt{v_i^T (M^T M)^{-1} v_i} < 1 \Rightarrow \text{Re}[\lambda(GG^{-1})] > 0$$

K' Bound

From ID: $\hat{G} = U \Sigma V^T \approx \sum_{i=1}^n \sigma_i u_i v_i^T$ $M = \begin{bmatrix} m_1 & \dots & m_n \\ \vdots & & \vdots \\ m_1 & \dots & m_n \end{bmatrix}$ Design M or M^T M to satisfy bound

$a_i = c \frac{\|u_i\|}{\sigma_i}$

Sidebar: Upper Bound that Ensures Integral Controllability

Only know G with uncertainty - Integral controllability satisfied if for all D in D

$$\sum_{i=1}^n \frac{\|u_i\|}{\sigma_i} \|D v_i\| < 1$$

Use $D = [D] \begin{bmatrix} d_1^r & \dots & d_1^i \\ \vdots & & \vdots \\ d_n^r & \dots & d_n^i \end{bmatrix}$ Use $D = [D] \begin{bmatrix} d_1^r & \dots & d_1^i \\ \vdots & & \vdots \\ d_n^r & \dots & d_n^i \end{bmatrix} \leq c^2, 1 \leq k \leq n$
 $c^2 = \lambda^2 n F_{\alpha}(n, t-n) = \sigma_{\alpha}^2 \chi_{\alpha}^2(n)$

Worst-case model uncertainty: $\max_{m \in D} \sum_{i=1}^n \frac{\|u_i\|}{\sigma_i} \|D v_i\| = \sum_{i=1}^n \frac{\|u_i\|}{\sigma_i} \sqrt{v_i^T (M^T M)^{-1} v_i}$ Select M or M^T M to satisfy: $\sum_{i=1}^n a_i \sqrt{v_i^T (M^T M)^{-1} v_i} < 1$

References:
 Garcia, C.E. and Morari, M. (1985). Internal Model Control: 2. Design for Multivariable Systems. *Ind Eng. Chem. Process Des. Dev.*, 24, 472-484.
 Koung, C.W. and MacGregor, J.F. (1994). Identification for Robust Multivariable Control: The Design of Experiments. *Automatica*, 30(10), 1541-1554.
 Skogestad, S. and Morari, M. (1987). Configuration Selection for Distillation Control. *AIChE Journal*, 33, 1620-1635.
 Darby, M.L. and Nikolaou, M. (Submitted for publication). Multivariable System Identification for Integral Controllability. *Automatica*.

Implications for Input Design

Let $M^T M = P \Lambda P^T$, $\Lambda = \begin{bmatrix} \lambda^1 & & \\ & \ddots & \\ & & \lambda^n \end{bmatrix}$ Consider fixed Λ - fixed information content

Minimize worst case bound
 $\min_{w_i} \sum_{i=1}^n a_i \sqrt{v_i^T (M^T M)^{-1} v_i} = \min_{w_i} \sum_{i=1}^n a_i \sqrt{w_i^T \Lambda^{-1} w_i} = \sum_{i=1}^n \frac{a_i}{\sqrt{\lambda_i}}$ $0 < a_1 < \dots < a_n$
 $0 < \lambda_1 < \dots < \lambda_n$

Recover rotated inputs: $\xi = W m$
 $P^T m = \Pi V$ (col V rearranged)
 Integral controllability satisfied $\sum_{i=1}^n \frac{a_i}{\sqrt{\lambda_i}} < 1$
 Time to achieve integral controllability $\sum_{i=1}^n \frac{a_i}{\sqrt{\lambda_i}} < 1 \Rightarrow T \geq \sum_{i=1}^n a_i / \sqrt{\text{var}(\xi_i)} + 1$

Time bound: $T = c^2 \text{IC}_{\text{opt}} + 1$

Implications for Input Design: Selecting λ_k - Analytical Solutions

Motivated by MPC, lump input and output variances into a weighted sum
 $\sum_{i=1}^n \text{var}(m_i) + (1-\alpha) \sum_{i=1}^n \text{var}(y_i) = \frac{1}{1-\alpha} \left(\sum_{i=1}^n \alpha \lambda_i^2 + (1-\alpha) \sum_{i=1}^n \lambda_i^2 \right) 0 \leq x \leq 1$

Consider following optimization problem:
Minimize variance s.t. IC bound $\min_{\lambda_i} \sum_{i=1}^n \lambda_i^2$ s.t. $\sum_{i=1}^n \frac{a_i}{\sqrt{\lambda_i}} \leq 1 - \epsilon$
 Solution (satisfies: $0 < \lambda_1 < \dots < \lambda_n$):
 $\lambda_k^* = \frac{1}{1-\epsilon} \left(\frac{a_k}{\lambda_k} \sum_{i=1}^n (a_i b_i) \right)^{1/2} = \frac{\lambda_k^* (x)}{\lambda_k^* (x)} = \frac{\alpha x^2 + (1-x) \lambda_k^2}{\alpha x^2 + (1-x) \lambda_k^2} = \frac{\alpha x^2 + (1-x) \lambda_k^2}{\alpha x^2 + (1-x) \lambda_k^2}$

$x=1$ $\lambda_k^2(1) \frac{\sigma_i^2}{\sigma_i^2}$ (output penalty only) $\lambda_k^2(1) \frac{\sigma_i^2}{\sigma_i^2}$ agrees with Koung-MacGregor
 $x=0$ $\lambda_k^2(0) \frac{\sigma_i^2}{\sigma_i^2}$ (input penalty only) $\lambda_k^2(0) \frac{\sigma_i^2}{\sigma_i^2}$ less aggressive than Koung-MacGregor

Design example s.t. IC & variance bounds $\max_{\lambda_i} \sum_{i=1}^n \lambda_i^2$ s.t. $\sum_{i=1}^n \frac{a_i}{\sqrt{\lambda_i}} \leq 1 - \epsilon$
 Solution (satisfies: $0 < \lambda_1 < \dots < \lambda_n$):
 IC bound inactive: $\lambda_i = \frac{a_i}{b_i}$ IC bound active: $\lambda_i = \frac{a_i}{b_i} \frac{\sigma_i^2}{\sigma_i^2}$ $\frac{\sigma_i^2}{\sigma_i^2} = \delta$, $r > 0$

Example 2×2 case: $\sigma_1 = 1, \sigma_2 = 0.5$, $\epsilon = 0.8$
 (c: input & output penalty) $c = 0.32$

Parameter accuracy better with ICmin
 Note: Both achieve integral controllability at $t = 5$

Use of Integral Controllability Bound to Determine Experimental Time

Using expression from earlier: $T = c^2 \left(\sum_{i=1}^n \frac{\|u_i\|}{\sigma_i} \sqrt{\text{var}(\xi_i)} \right)^2 + 1$

Simulate 100 experiments based on min variance s.t. IC bound for $x=0$ & $x=1$ (same IC bound for each)

Skogestad/Morari Column
 $G = \begin{bmatrix} 87.8 & -86.4 \\ 108.2 & -109.6 \end{bmatrix}$

Time bounds calculated for different confidence levels
 Time bound is conservative

General Formulation for Input Design - Numerical Solution

Cannot assume $0 < \lambda^1 < \dots < \lambda^n$ for general case: Solve numerically

- Split out time dependency $\sum_{i=1}^n \frac{\|u_i\|}{\sigma_i} \sqrt{v_i^T (M^T M)^{-1} v_i} = \sum_{i=1}^n \frac{\|u_i\|}{\sigma_i} \sqrt{w_i^T \Lambda^{-1} w_i}$
- Optimize wrt covariance of rotated inputs
- Time bound from optimal result

General Formulation
 Time bound: $T = c^2 \text{IC}_{\text{opt}} + 1$
 α $w_i w_j = \delta_{ij}$ orthogonality
 $\|V W \Lambda W^T V^T\| \leq \text{var}(y)$ individual input variance bounds
 $\|T W \Lambda W^T T^T\| \leq \text{var}(y)$ individual output variance bounds
 $T = [t_1 \dots t_n] \begin{bmatrix} u_1 & & \\ & \ddots & \\ & & u_n \end{bmatrix}$
 $W = [w_1 \dots w_n]$

Example

$G = \begin{bmatrix} 87.8 & -86.4 \\ 108.2 & -109.6 \end{bmatrix}$ $\text{var}(m_1) \leq 0.15$, $\text{var}(m_2) \leq 1.5$, $\text{var}(y_1) \leq 5.0$, $\text{var}(y_2) \leq 5.0$

Design	IC	det(cov(m))	λ_1/λ_2
ICmin	1.30*	6.08E-5	38.3
PRBS	4.70	4.44E-8	1.01
KM	2.05	4.47E-6	142

By correlating rotated inputs, ICmin operates at 2 bounds vs. 1
 ICmin achieves lower IC & higher determinant

$\text{cov}(\xi_{\text{opt}}) = \bar{\Lambda} = \begin{bmatrix} 2.04E-4 & 2.01E-4 \\ 2.01E-4 & 2.99E-1 \end{bmatrix}$
 A: active constraint

Time Realizations

$G = \begin{bmatrix} 87.8 & -86.4 \\ 108.2 & -109.6 \end{bmatrix}$ $\sigma_{m_1}^2 = 1$ for both outputs
 Simulate for 50 time steps
 Start id at $t = 5$
 True model used
 Steady-state, no dynamics
 Generate correlated output inputs: $\xi = Q^* x$, $Q^* Q = \bar{\Lambda}$
 x from PRBS with $\text{cov}(x) = I$

Parameter accuracy better with ICmin
 Note: Both achieve integral controllability at $t = 5$

Ongoing Work

- Larger systems - FCC (5x5) example
- Dynamic case - apply PRBS design to z based on estimates of open-loop dynamics:
 $\text{cov}(z) = I, \xi = Q^* z, Q^* Q = \bar{\Lambda}$
- Constrained case with min/max outputs and inputs (not just variances)

Conclusions

- Mathematical framework for designing experiments for $n \times n$ systems
- No need to classify systems as ill- or well-conditioned
- Algebraic in nature, allowing rigorous formulation of optimization problems
- Recover previous design results and propose new ones
- Optimal experiments for typical situations lead to correlated rotated inputs

Future Work

- Application to adaptive design of experiments (do not know true plant)
- Rigorous extension to dynamic models
- Incorporate IC bound into closed-loop testing schemes
- Apply to non-square systems (meaningful for MPC)
- Distribution of experimental time, Probabilistic stability formulations